Oxidation of CO

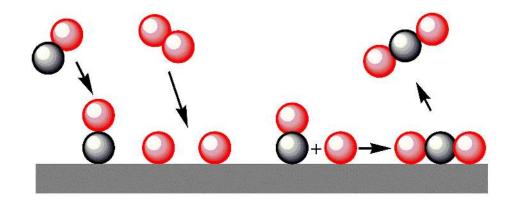
 $2CO + O_2 \rightarrow 2CO_2$

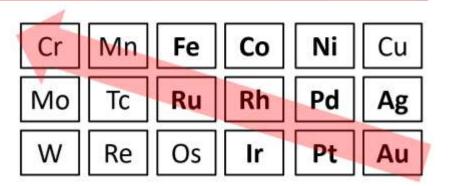
Conditions

- Catalyst should dissociate O_2 but leave C=O triple bond intact
- Catalyst should keep CO adsorbed and allow CO₂ to desorb

Suitability of metal catalyst

- Au is too unreactive and cannot dissociate O₂; Cr/Mo/W too reactive, dissociate CO and also bind O-atoms too strong making them unreactive
- **Pt** and **Pd** are suitable catalysts: intermediate reactivity





Automotive exhaust catalysis

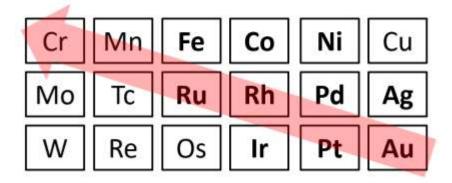
 $2CO + 2NO \rightarrow 2CO_2 + N_2$

Conditions

• Catalyst should dissociate NO but leave C≡O triple bond intact

Suitability of metal catalyst

- Fe, Co, Ni and Ru dissociate CO and NO; Pt does not dissociate NO
- Pd and Rh are suitable catalysts: intermediate reactivity

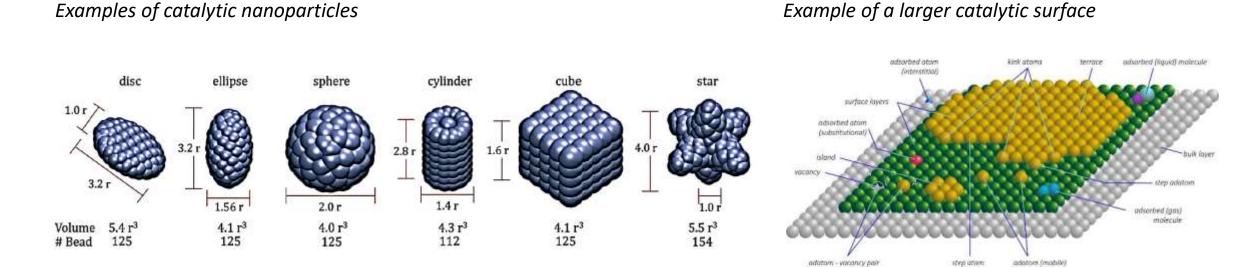


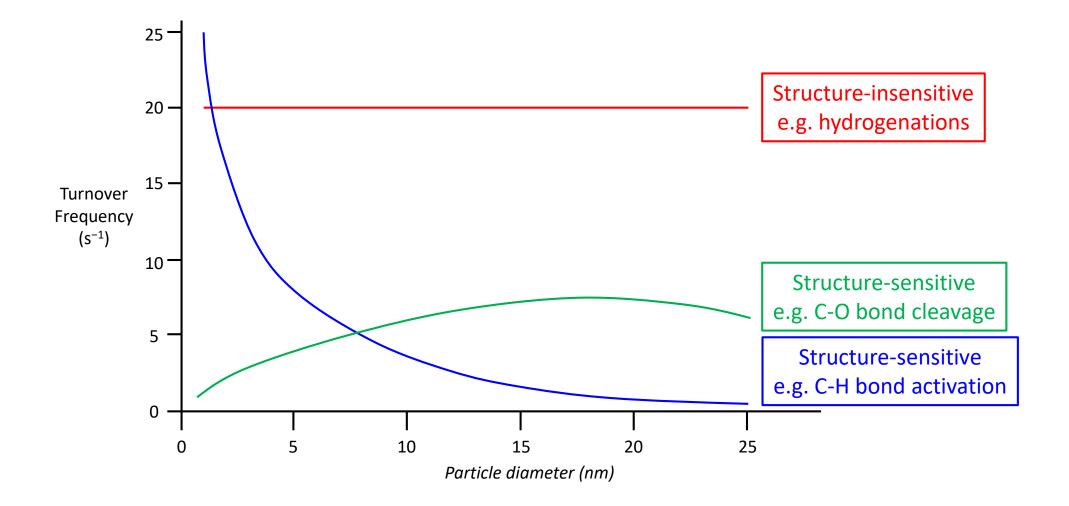
Structure-sensitive reaction

Turnover rate per catalyst surface atom depends on particle size and geometry

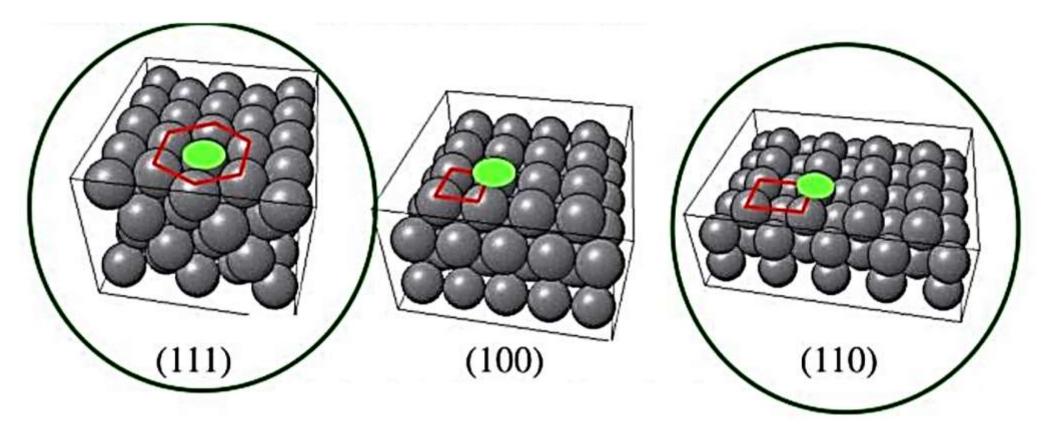
Structure-insensitive reaction

Turnover rate per catalyst surface atom independent of particle size – every surface atom is equally active



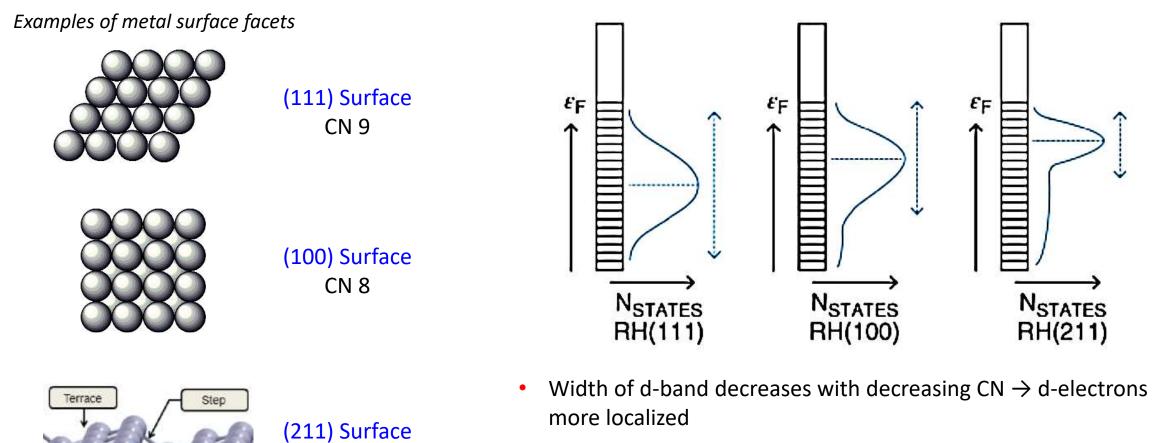


Main "low-index" surfaces



- Surfaces are regions of high energy
- The more close-packed a surface (the higher the coordination number), the lower the surface energy (more stable)

Electron density of reactive surface metal atom depends on atom topology and coordination number (CN)

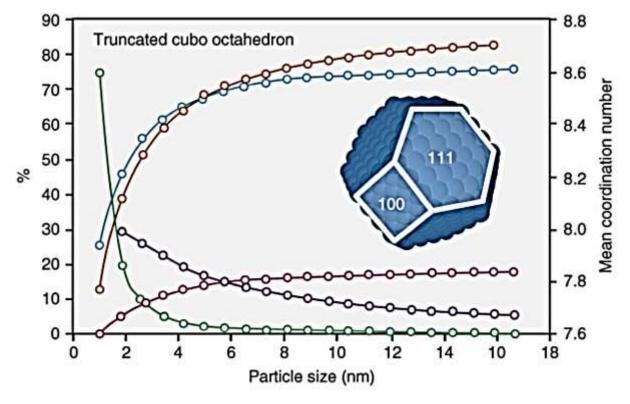


CN 7

 Average energy of d-band increases with decreasing CN → more overlap with orbitals of adsorbates → stronger bonding with adsorbates

Example: cleavage of an alkane C-H σ -bond

- Occurs at a single metal atom
- E^{act} is low if transition state (C-H bond nearly cleaved at metal atom) is stabilized
 - \rightarrow benefits from decreasing CN of metal atom
 - \rightarrow occurs when metal particles become smaller

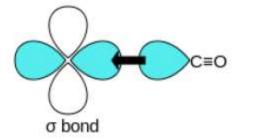


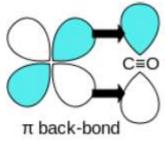
Catal. Rev. 2010, 52, 106

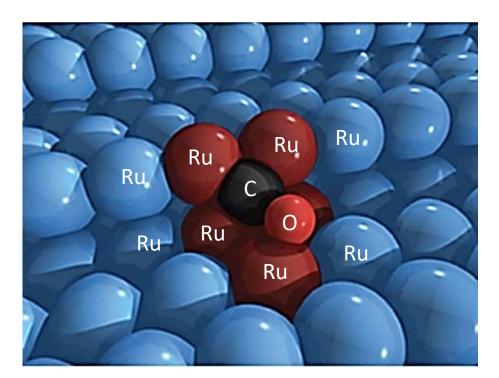
-o- % corner -o- % edge -o- % (100) -o- % (111) -o- Mean coordination number

Example: cleavage of a π -bond (CO, N₂, NO, etc.)

- Preferentially occurs at an ensemble of metal atoms at a surface step
- Dissociation of CO at planar **Ru**: $E^{act} > 200$ kJ/mol; at **Ru** step: < 100 kJ/mol
- Transition state: CO atoms bind at different metal atoms → stronger individual binding and no bending CO needed
- Bond breaking activated by π -back bonding from metal into antibonding of C-O bond
- Coverage of step edges by inactive **Au** atoms drastically poisons the catalyst







Support effects

Catalytic nanoparticles are usually deposited on porous support material: maintains high surface area

Electronic interactions

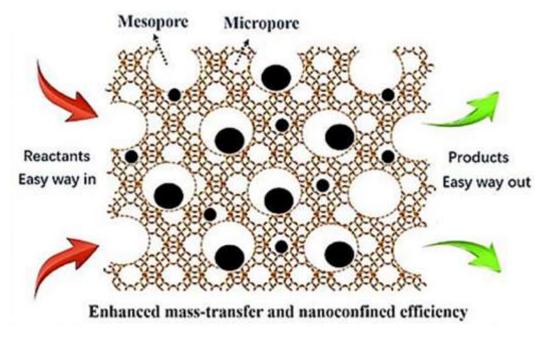
- Metal particles on semiconductors (e.g. TiO₂): direct chemical interaction via electron transfer between support and d-band of metal possible
- Metal particles on insulators (e.g. Al₂O₃, SiO₂): inductive interaction with metal; ions of support may change position d-band (only with small metal particles)

Structural interactions

Support may influence nanoparticle shape (depending of support-particle interaction strength)

Complications

- Support may diffuse over/encapsulate nanoparticle
- Support may react with nanoparticle (e.g. $Ni + \frac{1}{2}O_2 + Al_2O_3 \rightarrow NiAl_2O_4$)



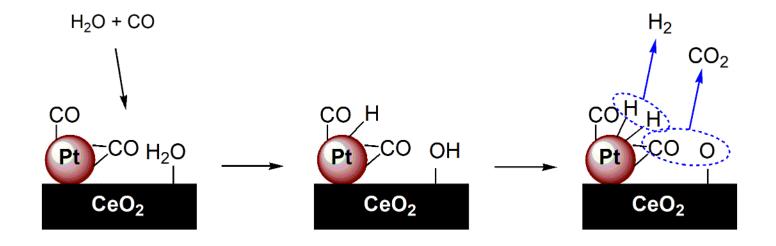
Support effects

Supports that participate in the catalytic reactions (bifunctional catalyst)

- Support and catalyst contribute to the catalytic steps
 - (1) Reactions occur at the interface of nanoparticle and support
 - (2) Diffusion of reactive species over both nanoparticle and support ("spillover")
 - (3) Both metal catalyst and support catalyze reactions

Example of (3): water-gas shift reaction

- $CO + H_2O \implies CO_2 + H_2$
- CO activated by **Pt** nanoparticles, H₂O by a hydrophilic metal-oxide support (here CeO₂)



Unsupported metal catalysts

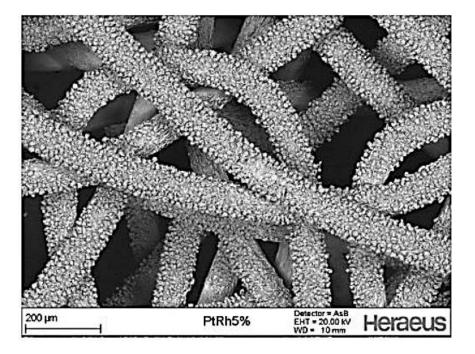
Examples:

NH₃ oxidation over Pt/Rh

- $NH_3 \rightarrow NO_x \rightarrow HNO_3$
- Catalyst: **Pt-Rh** wires (Ø 50 μm)
- Reaction at 800 °C: extreme rates, limited number of surface sites needed

Raney-Ni

- Hydrogenation catalyst
- Ni-catalyst itself is made porous (100 m²/g)
- Possible because **Ni** is cheap



Zeolites

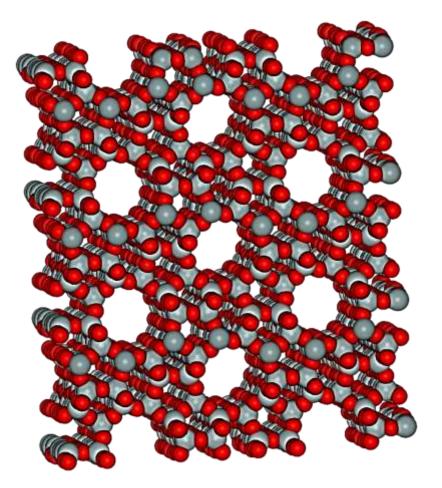
Porous organic materials based on non-heavy metal atoms

- Natural and synthetic
- Pore/channel sizes of 1 10 Å: fits small molecules
- Huge internal surface area of hundreds of m²/g
- Al/Si zeolites can act as strongly acidic Brønsted catalysts
- Pore size can lead to shape/size-selective reactions

Examples of applications

- Isomerizations, e.g. 1,3-dimethylbenzene to 1,4-dimethylbenzene
- Cracking of petroleum
- Conversion of methanol to hydrocarbon fuels

 $\begin{array}{l} 2\mathsf{CH}_3\mathsf{OH} \xrightarrow{} \mathsf{CH}_3\mathsf{OCH}_3 + \mathsf{H}_2\mathsf{O} \\ 2\mathsf{CH}_3\mathsf{OCH}_3 + 2\mathsf{CH}_3\mathsf{OH} \xrightarrow{} \mathsf{C}_6\mathsf{H}_{12} + 4\mathsf{H}_2\mathsf{O} \\ 3\mathsf{CH}_3\mathsf{OCH}_3 \xrightarrow{} \mathsf{C}_6\mathsf{H}_{12} + 3\mathsf{H}_2\mathsf{O} \end{array}$



ZSM-5 (Na_n[Al_nSi_{96-n}O₁₉₂].≈16H₂0)

Some applications

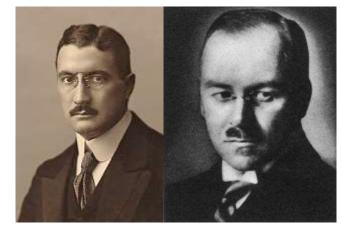


Fischer-Tropsch process

Industrial synthesis of hydrocarbons from syngas

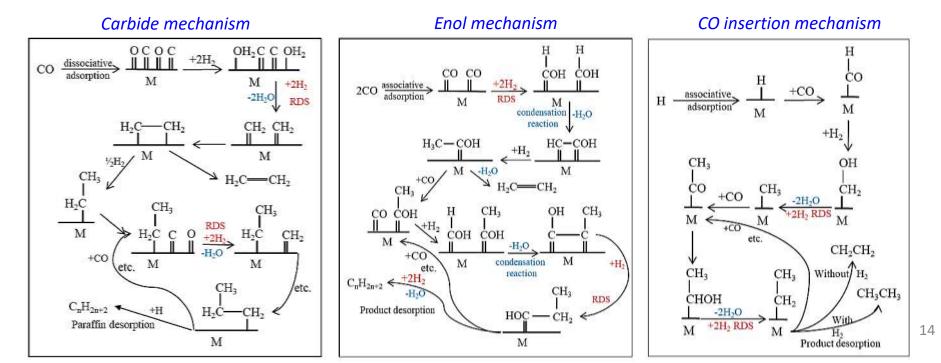
 $(2n + 1)H_2 + nCO \rightarrow C_nH_{2n+2} + nH_2O$ n = 10-20

- Developed in 1925
- Alternative to oil as the source of hydrocarbons
- Mainly **Fe**-based and **Co**-based solid catalysts
- Mechanism(s) still under debate



Franz Fischer

Hans Tropsch



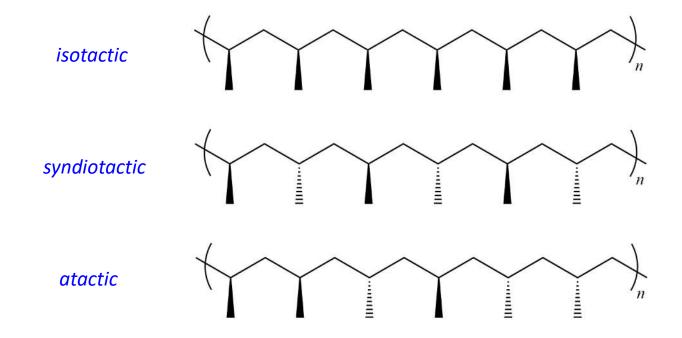
Catalysts 2019, 9, 259

Ziegler-Natta process

Industrial polymerization of alkenes

- Developed in 1953-1954. Nobel Prize 1963 •
- Polymerization of ethene into polyethylene at relatively low pressures
- **TiCl₄**-based catalysts on MgCl₂ solid support (similar crystal structures) •
- Formation of stereoregular polymers possible .



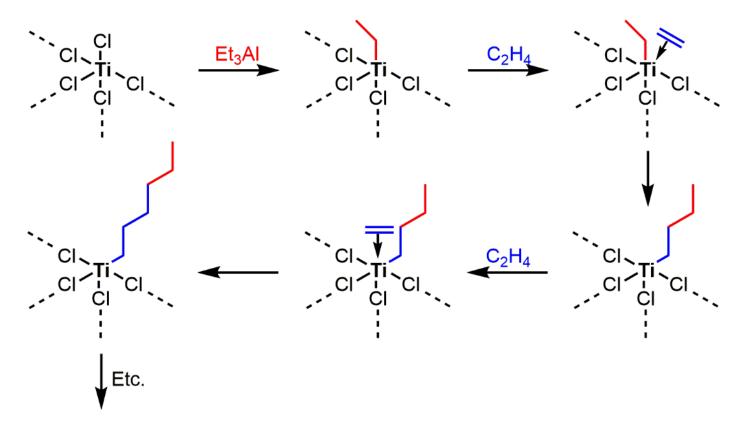


Giulio Natta

Ziegler-Natta process

Mechanism

• Alkene polymerization catalyzed at a surface **Ti(III)** center with a terminal Cl and a vacant coordination site

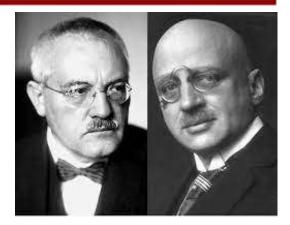


• In case of propene polymerization: isotactic polymer is obtained, controlled by specific surface structure of catalyst

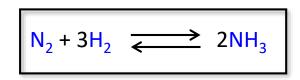
Haber-Bosch process

Industrial synthesis of ammonia from nitrogen and hydrogen

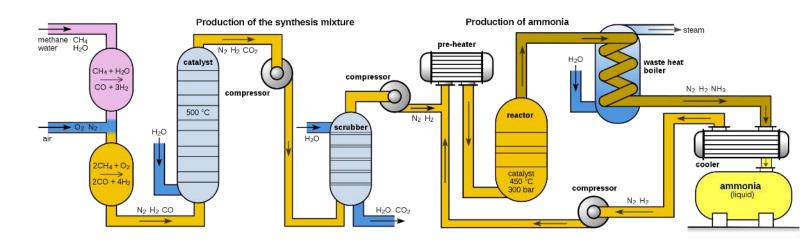
- Developed in 1909. Nobel Prizes Chemistry Haber in 1918 & Bosch in 1931
- Developed to produce fertilizer.....and explosives
- First: **Fe**-based solid catalysts. Nowadays **Ru** catalyst on carbon support



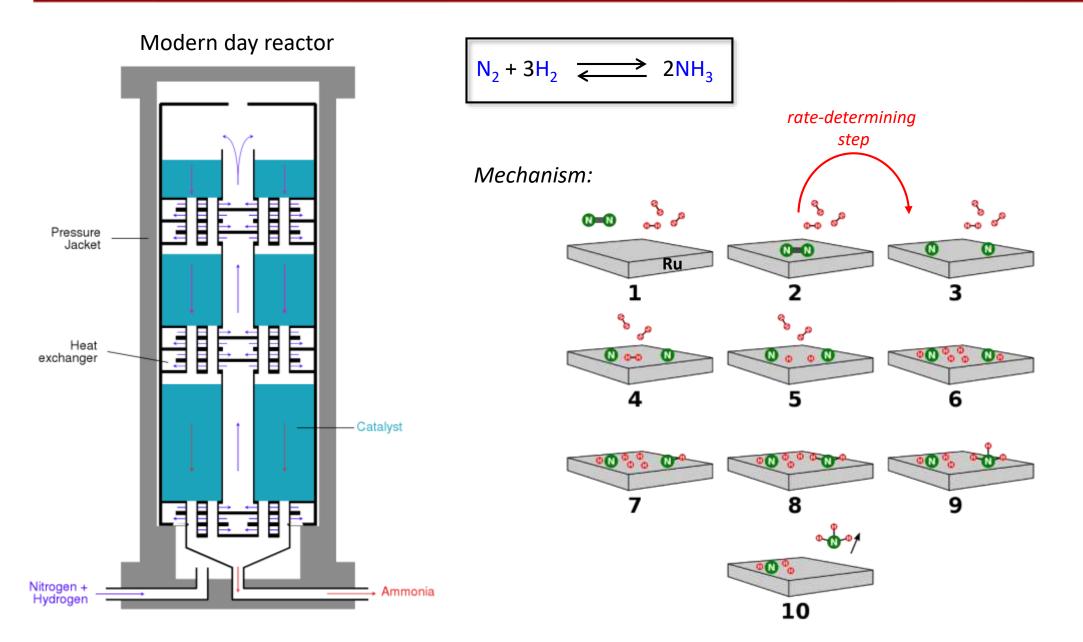
Carl Bosch Fritz Haber



 Exothermic equilibrium reaction with negative entropy: high pressure of >200 atm) needed but relatively low temperature of 400-500 °C (uncatalyzed reaction: 3000 °C)



Haber-Bosch process



Catalytic converters

Reduce emission of harmful gases from car exhaust

 $2CO + O_2 \rightarrow 2CO_2$ $C_3H_8 + 5O_2 \rightarrow 3CO_2 + 4H_2O$ $2NO + 2CO \rightarrow 2CO_2 + N_2$ $2NO + 2H_2 \rightarrow N_2 + 2H_2O$ $C_3H_8 + 10NO \rightarrow 3CO_2 + 4H_2O + 5N_2$

Pd or Pt catalyst Pd or Pt catalyst Rh catalyst Rh catalyst Pt catalyst



- >90% efficient in reducing emissions
- Honeycomb ceramic structure coated in finely divided Al₂O₃ ("washcoat")
- Fine particles (1 2 nm) of catalytic **Pt**, **Pd**, **Rh** dispersed in the cavities of the washcoat
- Lead-free fuel required Pb binds to Al₂O₃ washcoat
- Air : fuel ratio (about 15:1) is crucial
 - Ratio too high: O₂ competes with NO for H₂-oxidation
 - Ratio too low: CO and C₃H₈ will compete for O₂

Learning goals & study material

Learning goals

- You understand the basic reaction steps of heterogeneous catalysis
- You know the difference between physisorption and chemisorption and the theory of the respective bonding modes of molecules and atoms to a metallic surface
- You understand the qualitative thermodynamics and kinetics of heterogeneous catalysis on metals
- You understand the dependence of heterogeneous catalysis on microscopic surface structure and catalyst support
- You can apply the above knowledge to simple chemical reactions that are heterogeneously catalyzed

Study material

- These lecture slides
- Catalysis: An Integrated Textbook for Students (U. Hanefeld & L. Lefferts, Eds): Sections: 2.1, 2.1.1, 2.1.2.2, 2.1.3, 2.2, 2.2.1, 2.2.2, 2.2.3, 2.2.4, 2.4.1.1, 2.4.1.2, 2.4.1.3
- Only for background reading: Sections: 2.1.2, 2.1.2.1, 2.1.2.3